

## BACKGROUND OF THE INVENTION

The present invention relates to a device and method for determining biological heat potential, more specifically to the above-mentioned device and method concerning the autothermal thermophilic aerobic treatment (ATAT) system for wastewater and sludge treatment.

The key problems encountered in the conventional biological wastewater treatment of high-strength wastewaters include high excess sludge yield, low degradation rate, and the low organic loading. An autothermal thermophilic aerobic wastewater treatment (ATAT) system can be used to solve these problems. The ATAT system is normally operated under the aerobic conditions and at temperatures of 45-65°C, differing from those of mesophilic anaerobic treatment at 35°C or thermophilic aerobic treatment at 55°C. According to the van Hoff-Arrhenius' law, reaction rates easily increase at high temperatures. Moreover, according to bioenergetics, the energy capture efficiency of biomass decreases as the temperature increases, thus increasing the biological reaction temperature will increase the energy part for cell maintenance and simultaneously decrease the part for cell synthesis. Thus, the high temperature of an ATAT can reduce the sludge yield and increase the heat released from maintenance energy.

The current difficulties or misconception in the design of an ATAT system

include: requiring costly supplemental heat if the reaction fails to be spontaneous, and limitation of oxygen transfer rate at high degradation rate as dissolved oxygen (DO) concentration decreases at high temperatures. However, in 1990, the United State Environmental Protection Agency (USEPA) reviewed  
5 35 sets of full-scale operating data of autothermal thermophilic aerobic sludge digestion (ATAD) process in Europe and determined that the ATAD is a promising technology for municipal sludge. In Taiwan, ROC, we demonstrated the successful operation of a full-scale ATAT process treating food-processing oily wastewater. Therefore, the ATAT process of high strength wastewater in  
10 full-scale was evidenced. However, it requires a reliable device and method to accurately determine the biological heat potential of the wastewater (or sludge) for the successful design and operation of the ATAT process.

If a conventional chemostat is used to evaluate the heat potential of the ATAT process, the problems encountered are: 1. difficulty to evaluate the  
15 reaction spontaneity since the system normally results in a large amount of heat loss via poor insulation and aeration; 2. difficulty to overcome the high oxygen transfer rate required by the high degradation of substrate for the ATAT by using a conventional air diffusion system; 3. inaccuracy and time-consuming in the determination of monitoring parameters, such as chemical oxygen demand  
20 (COD), biological oxygen demand (BOD), and oxygen uptake rate (OUR) by conventional laboratory methods, particularly for on-line sensing.

## SUMMARY OF THE INVENTION

The present invention overcomes the difficulties as described above by providing a device and method for determining the biological heat potential and  
25 monitoring of heat flux and biological oxygen depletion, particularly for the



mainly consists of six units: a reactor, an oxygen controller, an internal heat controller, an external temperature controller, a mixing controller, and a signal and data controller. The device focuses on the programmable on-line and real-time capability for monitoring a large set of transient oxygen uptake data, heat compensation data, and surrounding temperature data. It also provides a method to use the device as mentioned above to determine the specific biological heat potential ( $h_b$ ) via the heat balance computer algorithm for the ATAT system.

### BRIEF DESCRIPTION OF THE DRAWINGS

The drawings disclose an illustrative embodiment of the present invention which serves to exemplify the various advantages and objects hereof, and are as follows:

Figure 1 shows the block diagram illustrating the main parts and their relations for the device of the present invention for determining the biological heat potential;

Figure 2 shows the diagram illustrating the acclimation apparatus of the present invention, which provides the necessary aerobic culture for the ATAT test;

Figure 3 shows the diagram illustrating the device of the present invention, used to determine the biological heat potential for the ATAT test;

Figure 4 shows the results of the oxygen uptake data fed on the glucose sample, obtained with the device of the present invention; and

Figure 5 shows the results of heat compensation data fed on the glucose sample as the substrate (energy source), obtained with the device of the present invention.

## DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENT

According to Figure 1, it is shown that the present invention provides a device and method for determining the biological heat potential. The device consists of an acclimation apparatus 10 for incubating an aerobic culture which is used as the source culture to a reactor 11 for carrying out the desired biological reactions, an external temperature controller 13a can be used to control and heat the ambient air surrounding the reactor 11 at a preset temperature for reducing the heat loss flux during the biological reaction, an oxygen controller 12 to provide and control the oxygen depleted within the reactor 11 with an on-line and real-time output of oxygen uptake data ( $O_u$  vs.  $t$ ), an internal heat controller 13b to control and heat the content of the reactor 11 at a preset temperature with an on-line and real-time output of heat compensation data ( $H_c$  vs.  $t$ ). Based on the above oxygen uptake data and heat compensation data, the method uses a specific biological heat potential evaluator 14 to compute the specific biological heat potential ( $h_b$ ) and the heat loss flux ( $J_o$ ). The method also uses a heat compensation ratio evaluator 15 to compute a transient heat compensation ratio ( $r$ ), and a minimal heat compensation ratio ( $r_{min}$ ) for evaluating an ATAT system.

### Derivation of the specific biological heat potential algorithm

The specific biological heat potential ( $h_b$ ) of this invention is defined as the released heat of a biological reaction per unit of substrate degraded in terms of biological oxygen demand (BOD), in the unit of kcal/g BODr. It is an important parameter for the design and operation of an ATAT system. The parameter can be included into a heat balance mathematical analysis for evaluating the reaction spontaneity and operating temperature of an ATAT system. For a biological reaction system at steady-state ( $dT/dt = 0$ ), with the use

of the internal heat controller and the external temperature controller, the heat balance analysis around the system can be established by the reaction term, the heat loss term, and the heat compensation term, as follows:

$$0 = \underbrace{h_b \frac{dO_u}{dt}}_{\text{reaction}} - \underbrace{J_o}_{\text{loss}} + \underbrace{\frac{dH_c}{dt}}_{\text{compensation}} \quad (1)$$

where  $h_b$  being the specific biological heat potential in the unit of kcal/g BODr,  $O_u$  being the accumulated oxygen uptake in the unit of g BODr,  $J_o$  being the heat loss flux in the unit of kcal/min, and  $H_c$  being the accumulated heat compensation data in the unit of kcal. Using an initial condition: at  $t = 0$ ,  $O_u = 0$  and  $H_c = 0$ , Equation (1) can be integrated into

$$H_c = J_o t - h_b O_u \quad (2)$$

Using the device of the present invention, the on-line real-time oxygen uptake data ( $O_u$  vs.  $t$ ) and the heat compensation data ( $H_c$  vs.  $t$ ) can be measured. These data can be incorporated into Equation (2) and analyzed by a multiple linear regression method based on the least-squared method for determining the specific biological heat potential ( $h_b$ ) and the heat loss flux ( $J_o$ ). During the period of reaction, a heat compensation ratio ( $r$ ) can be defined as follows:

$$r = H_c / J_o t \quad (3)$$

The magnitude of the  $r$  ratio is an indication of reaction spontaneity for the ATAT system. The smaller the  $r$ , the larger the extent of reaction spontaneity can be evidenced with the lab-scale ATAT system.

### **Acclimation apparatus**

The present invention provides an acclimation apparatus for incubating an aerobic culture, as shown in Figure 2. It consists of a 11 liter acclimation reactor 10b with a liquid volume of 10 liter, an air pump 16 and a diffuser 17 to maintain the dissolved oxygen (DO) concentration at 1 to 2 mg/L, a temperature probe 18 and a heater 19, incorporated with a proportional integrated derivative (PID) temperature controller 13b to maintain the acclimation reactor 10b at 55°C with a precision of 0.1°C, a heavy-duty magnate 20 driven by a magnetic stirrer 21 to maintain a homogeneous content within the acclimation reactor 10b, a reflux condenser 22 connected to the top the acclimation reactor 10b to prevent the loss of liquid solution via vaporization, a 4 liter substrate vessel 23 and a 4 liter nutrient vessel 24 to avoid the undesired substrate spoiling, and a peristaltic pump 25 to feed the acclimation reactor 10b operated at a preset flow rate and sludge retention time (SRT) for a treatment efficiency.

### **Example:**

#### **Acclimation operation**

Firstly, a 10 liter sludge is transferred from the aeration tank of a full-scale ATAT plant to the reactor of the acclimation apparatus. The reactor is fed on a glucose sample at a loading of 10 g/L COD and an SRT of 10 days. Effluent samples are periodically taken from the reactor for the analyses of COD, pH, and MLSS. Other performance characteristics are also observed for sludge settlability, culture color, forming, and microscope examination to determine the acclimation status.

The present invention allows for maintaining the normal acclimation operation to provide a stable source of seed culture required for the ATAT tests.

#### **ATAT test**

The ATAT test, as shown in Figure 3, consists of a reactor, an oxygen

controller, an internal heat controller, an external temperature controller, a mixing controller, and a signal and data controller capable of the on-line and real-time data acquisition of an oxygen uptake data and a heat compensation data. It can be used for an ATAT system and other biological reaction studies to  
5 obtain the specific biological heat potential based on the heat balance analysis.

As shown in Figure 3, the oxygen controller provides pure oxygen to maintain the oxygen content of the headspace of the reactor 30 at a preset value. The oxygen supply is regulated by a computer program with an on/off control mechanism 32. The oxygen source 33 will be turned on if oxygen level  
10 determined by the oxygen probe 31 is below the preset value and is turned off if above the preset value. Providing the oxygen is supplied at a constant rate, the on-time as recorded by the on-line and real-time computer program can be used to calculate the accumulated oxygen uptake data ( $O_u$  vs.  $t$ ). The carbon dioxide ( $\text{CO}_2$ ) stripper 34 is used to absorb the released  $\text{CO}_2$  resulting from the aerobic  
15 reaction by strong basic solution, such as potassium hydroxide (KOH). The internal heat controller uses an on/off control system, referring to the internal temperature probe 39 and the internal heater 40 to allow for operation of the reactor 30 at a constant temperature. Providing the heating power of the internal heater 40 is kept at constant, the on-line and real-time computer program can  
20 record the on-time of the internal heater 40 to calculate the heat compensation data ( $H_c$  vs.  $t$ ). The magnate 41 is driven by the magnetic stirrer 42 for high-strength mixing within the reactor 30 at a controllable speed to avoid spin-off. The signal and data controller, comprising a signal interface assembly 38 and a signal and data processor 43, consists of an on-line and real-time computer  
25 program, which can be used to monitor, control, and exhibit dynamic plots of the mixing speed, the reactor and surrounding air temperatures, the oxygen uptake data, and the heat compensation data. The external temperature controller



uses the temperature probe 37 connected to the external heater 44 to maintain at an appropriate constant surrounding temperature to reduce heat loss from the reactor 30. The ambient air surrounding the reactor 30 is circulated with a fan to maintain a homogeneous ambient temperature.

5        When operating the ATAT test, the seed culture is first transferred into the reactor 30 and then operated in a semi-continuous mode. The substrate (such as glucose) sample is daily fed after daily wasting of the excess sludge from the reactor 30 to control the ATAT test at a preset SRT. After reaching a steady state, a repeatable pattern of oxygen uptake data can be observed and the ATAT  
10      test is completed.

### **Results and Discussion**

Figures 4 and 5 show the  $O_u$  and  $H_c$  curves. It can be found that the  $O_u$  curve varied from day to day, and the  $H_c$  curve was more repeatable during one day of testing period. The  $O_u$  data and  $H_c$  data were analyzed with Equation (3)  
15      with a multiple linear regressed method to estimate the specific biological heat potential ( $h_b$ ) and the heat loss flux ( $J_o$ ) for comparison. The regression results indicate that the  $h_b$  normally ranges from 3.28-4.53 kcal/g BODr, with exception from the 3<sup>rd</sup> to 6<sup>th</sup> days. The  $R^2$  values of 0.92-0.95 for all the 8 testing days indicate good linearity, even for 3<sup>rd</sup> to 6<sup>th</sup> days. The reason for the wide  
20      variation of  $h_b$  from the 3<sup>rd</sup> to 6<sup>th</sup> days remains to be further investigated. It was speculated that it might be due to the dynamic nature of the thermophilic microbial system associated with incomplete acclimation under the testing conditions. It was not likely due to the mechanical problems of the ATAT system since  $h_b$  was automatically brought back to the base line values of the 1<sup>st</sup>  
25      to 3<sup>rd</sup> days at the 7<sup>th</sup> and 8<sup>th</sup> days.

The regression result also indicates that the heat loss flux ( $J_o$ ) varies in a fairly narrow range of 0.43-0.55 kcal/min. The heat loss flux reduces about 10%

when the system experienced lower biological heat on the 5<sup>th</sup> to 6<sup>th</sup> days.

Using the average  $h_b$  value (4.28 kcal/g BODr) and the average heat loss flux ( $J_o$ ) value (0.50 kcal/min), the heat compensation ratio can be determined to be with a minimum of 89.2% at 12 hours during the 24 hours of testing period.

5        The present invention provides a device for determining the biological heat potential by measuring the on-line real-time oxygen uptake data ( $O_u$  vs.  $t$ ) and heat compensation data ( $H_c$  vs.  $t$ ) from an ATAT test. The present invention also provides a data processing method to calculate the biological heat potential. The method uses a multiple linear regression algorithm to solve a governing  
10    function based on a heat balance model to determine the specific biological heat potential ( $h_b$ ) and the heat loss flux ( $J_o$ ) of the ATAT test. The results show that the present invention is a useful tool for an ATAT study. As the system is fed on 10-g COD/L glucose sample at an SRT of 10 days, the  $h_b$  is determined to be 4.28 kcal/g BODr. Moreover, the heat loss flux ( $J_o$ ) of the ATAT system is  
15    determined to be 0.50 kcal/min and the minimal heat compensation ratio ( $r_{min}$ ) is 89.2%.

Many changes and modifications in the above described embodiment of the invention can, of course, be carried out without departing from the scope thereof. Accordingly, to promote the progress in science and the useful arts, the  
20    invention is disclosed and is intended to be limited only by the scope of the appended claims.